

# CO<sub>2</sub> Hydrogenation to Methanol on a YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> Catalyst

L. Z. Gao and C. T. Au<sup>1</sup>*Chemistry Department and Center for Surface Analysis and Research, Hong Kong Baptist University, Kowloon Tong, Kowloon, Hong Kong, China*

Received January 4, 1999; revised May 11, 1999; accepted September 13, 1999

The synthesis of methanol from CO<sub>2</sub> and H<sub>2</sub> over YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> was studied. The aim was to clarify (i) the nature of the catalyst in the working state, (ii) the redox behaviour of copper in various oxidation states, and (iii) the formation and transformation of precursor species in methanol synthesis. The effects of reaction pressure, temperature, and space velocity on the catalytic performance were also investigated. The optimum reaction conditions were pressure = 3.0 MPa, space velocity = 3600 h<sup>-1</sup>, and temperature = 240°C. After H<sub>2</sub> reduction at 250°C, the YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> transformed from an orthorhombic to a tetragonal structure, a phase which is active for methanol synthesis. In a H<sub>2</sub>-reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample, there were Cu<sup>+</sup> and oxygen vacancies and electrons trapped at the oxygen vacancies. We observed that CO<sub>2</sub> adsorption would consume the trapped electrons, resulting in the reoxidation of Cu<sup>+</sup> to Cu<sup>2+</sup>. Intermediate species such as formate, methylenebisoxo, formyl, formaldehyde, and methoxide were observed in *in situ*-FTIR and FT-Raman studies; they were also captured by CD<sub>3</sub>I during methanol synthesis. Based on these experimental results, a reaction mechanism for CO<sub>2</sub> hydrogenation to methanol over YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> was proposed. In this mechanism, hydrogen adsorbs dissociatively at the Cu<sup>+</sup> sites of the CuO<sub>x</sub> planes, whereas CO<sub>2</sub> adsorbs at the oxygen vacancies. The spillover of hydrogen atoms from Cu<sup>+</sup> to the oxygen atoms and/or carbon atom of adsorbed CO<sub>2</sub> leads to the formation of COOH, COHOH, HCOHOH, and H<sub>2</sub>COHOH species; subsequently, one of the C–O bonds is weakened. Other intermediate species such as formate, methylenebisoxo, formyl, formaldehyde, and methoxide could be formed, and the final products are methanol, bimethyl ether, and CO. © 2000 Academic Press

**Key Words:** YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>; methanol synthesis; CO<sub>2</sub> hydrogenation mechanism.

## 1. INTRODUCTION

The synthesis of methanol over Cu/ZnO-type catalysts has been studied for years. However, several important questions remain unsolved. There are disagreements on (i) the working oxidation state of Cu, (ii) the roles of Cu and ZnO, (iii) the identity of the active sites, (iv) the structure of the catalyst, and (v) the reaction mechanism.<sup>14</sup>C labelling experiments under realistic industrial conditions

(50 bar, 250°C) suggested that the carbon in methanol is mainly from CO<sub>2</sub> in a CO/CO<sub>2</sub>/H<sub>2</sub> feed with a low CO<sub>2</sub>/CO ratio (1–5). However, it is believed that CO hydrogenation could be significant at a higher temperature (6). Numerous workers have found that the ratio of CO<sub>2</sub>/CO has clear effects on the rate of methanol formation (6–11). Klier and co-workers (12, 13) observed a maximum synthesis rate at CO<sub>2</sub>/CO = 1/14. They claimed that, at lower CO<sub>2</sub> concentrations, the catalyst was deactivated due to overreduction by H<sub>2</sub> and CO, and at higher CO<sub>2</sub> concentrations, the synthesis was retarded due to the strong adsorption of CO<sub>2</sub>. Lee and co-workers (11) found that an oxidized copper surface in a CO<sub>2</sub>/H<sub>2</sub> feed was more active and stable than an overreduced one in a CO/H<sub>2</sub> feed. Carbon dioxide has been considered to have a role to play in controlling the surface composition, oxidation state, and dispersion of copper in the catalysts. It has been suggested that the predominant site for methanol synthesis is (i) metallic Cu (14, 15), (ii) Cu<sup>+</sup> species in close contact with ZnO (16, 17), (iii) Cu<sup>0</sup>–Cu<sup>+</sup> couple (18), or (iv) the interface between Cu metal and the semiconductive ZnO support (19, 20).

Combined XRD/EXAFS spectra provided new insights into the structural changes during catalysis. Clausen *et al.* (21–23) found a reversible change in the apparent coordination number of the Cu atoms when the oxidation potential of the gas was changed. Specifically, it was observed that a significant increase in the coordination number for Cu occurred when the catalyst was exposed to a strongly oxidative gas. With a change back to a gas with lower oxidation potential, the coordination number decreased. The oxygen vacancies created in a reducing atmosphere may influence the structure and morphology of the catalyst, to which the catalytic activity is sensitive (24). Chinchin *et al.* (25, 26) proposed that the surface atomic oxygen O\* plays important roles in methanol synthesis by promoting the adsorption of CO<sub>2</sub> and participating in the hydrogenation steps. This aroused extensive theoretical research on the bonding of atomic oxygen to copper crystals (e.g., 27, 28). However, such effects of surface O\* could not be observed experimentally (29). Hydrogen spillover was proposed by Burch *et al.* (30). Most researchers considered formate species to be the intermediate in methanol synthesis (31–33). The formate species was also suggested to be an intermediate in

<sup>1</sup> To whom correspondence should be addressed. Fax: (852) 2339 7348. E-mail: pctau@hkbu.edu.hk.

formic acid decomposition and in water–gas shift (WGS) reactions over Cu-containing catalysts (34–36).

The material  $\text{YBa}_2\text{Cu}_3\text{O}_7$  is a well-known superconductor. The exceptionally wide range of oxygen nonstoichiometry and the high transport rate of oxygen make it a potentially attractive catalyst for oxidation. It has been used in oxidative reactions such as CO and light hydrocarbons oxidation to  $\text{CO}_2$ ;  $\text{CH}_4$  partial oxidation to CO,  $\text{CH}_3\text{OH}$ ,  $\text{CO}_2$ , and HCHO (37); and toluene oxidation to benzonitrile (38). It can also be used as a catalyst for NO direct decomposition or NO reaction with CO to produce  $\text{N}_2$  and  $\text{CO}_2$  (39, 40). The catalytic activities are closely related to the nature of  $\text{YBa}_2\text{Cu}_3\text{O}_7$ , such as defined structure, the high and regular dispersion of copper, the oxygen vacancies, and the bivalent or trivalent states of copper. We envisage that it can also be employed as a model catalyst to study  $\text{CO}_2$  and CO hydrogenations. In the present study, the hydrogenation of  $\text{CO}_2$  on  $\text{YBa}_2\text{Cu}_3\text{O}_7$  was reported. Temperature-programmed desorption (TPD), temperature-programmed surface reaction (TPSR), and pulse experiments were used to study  $\text{CO}_2$  adsorption and transient reactions. Techniques such as XRD, TG/DTA, temperature-programmed reduction (TPR), EPR, and XPS were employed to investigate the structure, copper oxidation state, and redox ability of  $\text{YBa}_2\text{Cu}_3\text{O}_7$ . *In situ*-FTIR and laser FT-Raman spectroscopies were used to explore the reaction intermediates. Similar studies of CO hydrogenation on  $\text{YBa}_2\text{Cu}_3\text{O}_7$  will be reported in a forthcoming paper.

## 2. EXPERIMENTAL

The  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample was prepared by grinding stoichiometric amounts of high-purity nitrates of yttrium, barium, and copper. The mixture was heated in air at  $600^\circ\text{C}$  for 5 h. The material was then pressed, crushed, and sieved to 100–140 mesh and calcined at  $900^\circ\text{C}$  for 10 h. The BET surface area of the catalyst was determined by using nitrogen adsorption data at  $-196^\circ\text{C}$  on a Nova 1200 system.

Methanol synthesis was conducted in a pressurized flow reactor. The reactor pressure was regulated by a back-pressure regulator. The catalytic performance was determined by placing 0.2 ml of catalyst into a microreactor connected to a gas manifold and operated with a feedstream containing a 3/1 mixture of  $\text{H}_2$  and  $\text{CO}_2$ . The products were analyzed by means of GC. Prior to each experiment, the fresh catalyst was reduced *in situ* at  $250^\circ\text{C}$  for 8 h in a  $\text{H}_2/\text{He}$  (1/4) stream flowing at  $60\text{ ml min}^{-1}$ .

Powder X-ray diffraction (XRD) studies were performed on a Rigaku D-Max Rotaflex diffractometer with  $\text{CuK}\alpha$  radiation and a Ni filter. X-ray diffraction data were collected at room temperature in the range of  $5^\circ$ – $80^\circ$ .

The  $\text{H}_2$ -TG/DTA measurements were carried out on a Rigaku thermoanalyzer. Fresh (nonreduced) sample (43 mg) was used. A mixture of 20%  $\text{H}_2$ –80% He (flow rate,

$20\text{ ml min}^{-1}$ ) was passed through the sample. The temperature range was from room temperature to  $700^\circ\text{C}$  and the heating rate was  $10^\circ\text{C min}^{-1}$ .

TPR was conducted by using a 10%  $\text{H}_2$ –90%  $\text{N}_2$  (v/v) mixture. The flow rate of the carrier gas was  $50\text{ ml min}^{-1}$  and a thermal conductivity detector was used. The amount of sample used was 0.2 g and the heating rate was  $10^\circ\text{C min}^{-1}$ . Before the TPR experiment was performed, the fresh sample was first calcined *in situ* at  $800^\circ\text{C}$  for 2 h under an oxygen flow of  $15\text{ ml min}^{-1}$ , followed by cooling in oxygen to room temperature. The reduced ( $\text{H}_2$ ,  $250^\circ\text{C}$ ) or used sample was first treated *in situ* at  $800^\circ\text{C}$  for 2 h under a He flow of  $15\text{ ml min}^{-1}$ , followed by being cooled in He to room temperature.

The dispersion of copper was determined on the basis of the measurement of  $\text{N}_2\text{O}$  decomposition at  $90^\circ\text{C}$  over the catalysts. The catalyst was reduced at  $250^\circ\text{C}$  in a mixture of 20%  $\text{H}_2$ –80% He for 8 h and purged with He for 2 h. The sample was then cooled down to  $60^\circ\text{C}$ . A quantity of  $\text{N}_2\text{O}$  was pulsed through the catalyst bed with He being the carrier gas. The surface concentration of Cu could be calculated according to the amount of  $\text{N}_2$  produced.

EPR spectra were recorded at  $-196^\circ\text{C}$  with a JEOL spectrometer operating in the X-band and calibrated with a DPPH standard ( $g=2.004$ ). The catalyst was placed in a self-made quartz cell in which the sample could be treated at various temperatures and atmospheres. For example, the sample could be treated in  $\text{CO}_2$  (flow rate,  $15\text{ ml min}^{-1}$ ) at  $250^\circ\text{C}$  for 2 h, followed by being purged with He at the same temperature and then quenched in liquid nitrogen before EPR analysis.

Photoelectron spectra were recorded with a SKL-12 spectrometer equipped with a  $\text{MgK}\alpha$  X-ray source. The residual pressure in the analysis chamber was maintained below  $10^{-9}$  Torr during data acquisition. The C(1s) peak at a binding energy of 284.6 eV was taken as an internal reference.

For TPD studies, the sample (0.2 g) was placed in the middle of a quartz microreactor with 4-mm i.d. The outlet gases were analyzed online by mass spectrometry (HP G1800A). The heating rate was  $15^\circ\text{C min}^{-1}$  and the temperature range was from room temperature to  $800^\circ\text{C}$ . Before the  $\text{O}_2$ -TPD experiments were performed, a fresh sample was heated in  $\text{O}_2$  at  $800^\circ\text{C}$  for 2 h and then cooled to room temperature in  $\text{O}_2$ . For a reduced sample, the sample was  $\text{H}_2$ -reduced *in situ* at  $250^\circ\text{C}$  for 8 h, cooled to room temperature in He, and then heated in He from room temperature to  $800^\circ\text{C}$  for  $\text{O}_2$ -TPD study. Before the  $\text{CO}_2$ -TPD experiments were performed, a fresh sample was first calcined *in situ* at  $800^\circ\text{C}$  for 2 h under a flow of oxygen ( $20\text{ ml min}^{-1}$ ) and then purged with helium to room temperature. For a reduced sample, it was first treated in helium for 2 h at  $800^\circ\text{C}$  and then cooled in He to room temperature. The  $\text{CO}_2$ -TPD experiment was performed according to the following procedures: the sample was kept in a flow of  $\text{CO}_2$  ( $20\text{ ml min}^{-1}$ ) for 1 h at a desired temperature and then cooled to room temperature

in CO<sub>2</sub>. After being He-purged at room temperature for 1 h, the sample was heated to 800°C in helium.

TPSR experiments were carried out on a microreactor system. About 0.5 g of catalyst was packed in the middle of a quartz tube. The sample was exposed to CO<sub>2</sub> at a desired temperature for 2 h and then cooled to room temperature in CO<sub>2</sub>, followed by He purging for 1 h. Then, the sample was heated to 700°C at a rate of 15°C min<sup>-1</sup> under a H<sub>2</sub> flow. The outlet gases were analyzed by means of mass spectrometry.

Pulse reaction was carried out on a pulse microreactor system. Each pulse volume was 67.5 μl. During the reaction, H<sub>2</sub> was used as the carrier gas (flow rate, 20 ml min<sup>-1</sup>).

A chemical-trapping experiment was performed during TPSR and CO<sub>2</sub>-pulsing experiments by injecting CD<sub>3</sub>I (0.2 μl) onto the sample. The products were analyzed by mass spectrometry.

*In situ*-FTIR spectra were collected on a Nicolet series II magna-IR 550 spectrometer with a SPECTRA TECH *in situ* cell. The catalyst powder weighing approximately 70 mg was contained in a low-dead volume infrared cell. The cell was heated by means of an electrical resistance heater. *In situ*-absorbance spectra were obtained at 4-cm<sup>-1</sup> resolution. The spectra were then referenced to a spectrum of the catalyst collected at the same temperature under a He or H<sub>2</sub> flow, as appropriate. Before FTIR spectrum collection, the cell was pumped for 5 min to remove gaseous CO<sub>2</sub> and H<sub>2</sub>.

Laser FT-Raman spectra were recorded using a Nicolet 560 FT-Raman spectrometer with a He-Ne laser operating at a power of 1 mW. Spectra were collected at a resolution of 4 cm<sup>-1</sup>. The sample (0.1 g) in a self-made quartz tube could be heated to 800°C and exposed to reactant gas without exposure to air.

### 3. RESULTS

#### 3.1. Catalytic Activities

We observed that a reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> catalyst was active in CO<sub>2</sub> hydrogenation whereas a fresh (nonreduced) one was not. Tables 1–3 show the effects of reaction temperature, pressure, and space velocity on the

TABLE 1

Effects of Reaction Temperature on the Catalytic Performance

Reaction temperature (°C)	CO <sub>2</sub> conversion (%)	Rate of CO <sub>2</sub> reaction (10 <sup>-3</sup> mol m <sup>-2</sup> h <sup>-1</sup> )	Products selectivity (%)		
			MeOH	DME	CO
200	0.9	1.1	72.5	5.8	20.1
220	1.2	1.4	71.3	5.5	23.2
240	3.4	3.8	50.7	3.4	45.9
260	4.4	4.8	34.8	2.5	62.7
280	4.6	4.8	30.6	2.1	63.4

Note. MeOH: methanol; DME: dimethyl ether. Reaction conditions: pressure = 3.0 MPa; GHSV = 3600 h<sup>-1</sup>; H<sub>2</sub>/CO<sub>2</sub> = 3 : 1 (molar ratio).

TABLE 2

Effects of Space Velocity on the Catalytic Performance

Space velocity (h <sup>-1</sup> )	CO <sub>2</sub> conversion (%)	Rate of CO <sub>2</sub> reaction (10 <sup>-3</sup> mol m <sup>-2</sup> h <sup>-1</sup> )	Products selectivity (%)		
			MeOH	DME	CO
1800	4.2	2.4	34.9	2.6	62.5
3600	3.0	3.4	38.4	3.3	58.3
5400	2.7	4.6	44.2	3.7	52.1
7200	1.8	4.1	48.9	4.1	47.0
9000	1.4	3.9	51.1	4.1	44.8

Note. MeOH: methanol; DME: dimethyl ether. Reaction conditions: pressure = 3.0 MPa; T = 240°C; H<sub>2</sub>/CO<sub>2</sub> = 3 : 1 (molar ratio).

catalytic performance. One can observe that the products of CO<sub>2</sub> hydrogenation over the catalyst are CO, CH<sub>3</sub>OCH<sub>3</sub>, and CH<sub>3</sub>OH. High pressure, high space velocity, and low temperature are favourable to methanol and CH<sub>3</sub>OCH<sub>3</sub> formations, whereas the opposite is true for CO formation. High pressure, high temperature, and low space velocity are favourable to CO<sub>2</sub> conversion. The reaction competitive to methanol synthesis is the RWGS (reverse water-gas shift) reaction. The BET surface area of the catalyst was 4.5 m<sup>2</sup> g<sup>-1</sup>.

#### 3.2. XRD, H<sub>2</sub> TG/DTA, and TPR

The XRD pattern of a fresh sample indicated that the material was single-phase and was orthorhombic in structure. It can be formulated as YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> (41). After reduction in H<sub>2</sub> at 250°C, it transformed to a tetragonal structure with the composition of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub>. There are Cu<sup>2+</sup> and Cu<sup>3+</sup> in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> (42), whereas there are Cu<sup>+</sup> and Cu<sup>2+</sup> in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub> (43). There should be oxygen vacancies generated in the lattice of tetragonal YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub>. Figure 1A shows the H<sub>2</sub>-TG/DTA curves of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>. There are two weight loss steps in the TG curve at ca. 240 and 420°C; the former is corresponding to an exothermic effect whereas the latter is to an endothermic effect. The transformation of phase from orthorhombic to tetragonal takes place at ca. 240°C. After reduction at 400°C, we found that the YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub> sample was broken down

TABLE 3

Effects of Reaction Pressure on the Catalytic Performance

Reaction pressure (Mpa)	CO <sub>2</sub> conversion (%)	Rate of CO <sub>2</sub> reaction (10 <sup>-3</sup> mol m <sup>-2</sup> h <sup>-1</sup> )	Products selectivity (%)		
			MeOH	DME	CO
0.5	2.0	0.4	12.1	0.8	87.4
1.0	2.7	1.0	27.6	3.2	69.2
2.0	3.0	2.3	38.4	3.3	58.3
3.0	3.4	3.8	50.7	3.4	45.9

Note. MeOH: methanol; DME: dimethyl ether. Reaction conditions: T = 240°C; GHSV = 3600 h<sup>-1</sup>; H<sub>2</sub>/CO<sub>2</sub> = 3 : 1 (molar ratio).

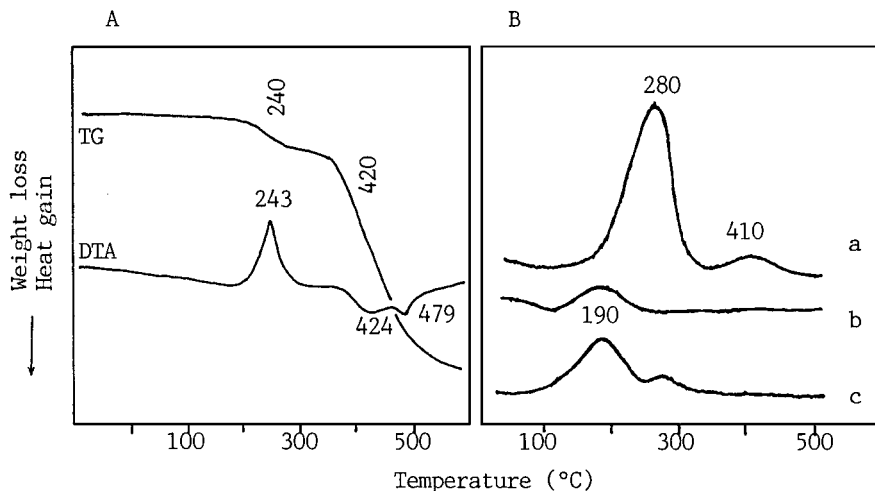


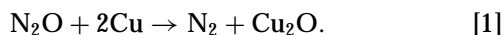
FIG. 1. (A)  $H_2$ -TG/DTA profiles for fresh  $YBa_2Cu_3O_7$ . (B) TPR curves for (a) fresh  $YBa_2Cu_3O_7$ , (b) reduced ( $H_2$ ,  $250^\circ C$ )  $YBa_2Cu_3O_7$ , and (c) reduced ( $H_2$ ,  $250^\circ C$ )  $YBa_2Cu_3O_7$  used for  $CO_2$  hydrogenation.

to a mixture of  $CuO$ ,  $Cu_2O$ ,  $Cu$ ,  $BaO$ , and  $Y_2O_3$ . Depending on the weight loss, the composition during reduction at  $250^\circ C$  was approximately  $YBa_2Cu_3O_{6.325}$ , which could also be speculated as  $YBa_2Cu^{2+}_{2.65}Cu^{+}_{0.35}O_{6.325}$  or  $YBa_2Cu^{0.175}Cu^{2+}_{2.825}O_{6.325}$ .

Figure 1B shows the TPR profiles of fresh  $YBa_2Cu_3O_7$ , reduced ( $H_2$ ,  $250^\circ C$ )  $YBa_2Cu_3O_7$ , and  $YBa_2Cu_3O_7$  used for  $CO_2$  hydrogenation. In profile 1B(a), there are a strong peak centered at ca.  $280^\circ C$  and a weak one at ca.  $410^\circ C$ . The former corresponds to the first weight loss and the latter to the second weight loss in the TG curve (Fig. 1A). Profile 1B(b) shows only one small peak at ca.  $190^\circ C$ , implying that after reduction at  $250^\circ C$   $YBa_2Cu_3O_{6.325}$  could still be reduced slightly at ca.  $190^\circ C$  and become  $YBa_2Cu_3O_{6.325-y}$ . This also means that the potential of oxygen mobility in tetragonal  $YBa_2Cu_3O_{6.325}$  is higher than that in  $YBa_2Cu_3O_7$ , while the content of mobile oxygen in  $YBa_2Cu_3O_{6.325}$  is less than that in  $YBa_2Cu_3O_7$ . Profile 1B(c) is the TPR profile of  $YBa_2Cu_3O_7$  used in a  $CO_2$  hydrogenation reaction. A strong reduction band at  $190^\circ C$  and a weak one at  $280^\circ C$  were observed, indicating that after  $CO_2$  hydrogenation the reduced catalyst was somewhat reoxidized.

### 3.3. $N_2O$ Titration

The concentration of surface  $Cu^0$  could be estimated according to the stoichiometric reaction of  $N_2O$  with metallic  $Cu$  at  $90^\circ C$  (44, 45):



However, the titration with  $N_2O$  at  $90^\circ C$  of a  $YBa_2Cu_3O_7$  sample  $H_2$ -reduced at  $250^\circ C$  showed no  $N_2$  formation. The result suggests that there was no metallic copper on the reduced sample. For a  $YBa_2Cu_3O_7$  sample  $H_2$ -reduced at  $400^\circ C$ ,  $N_2O$  titration at  $90^\circ C$  produced  $N_2$ .

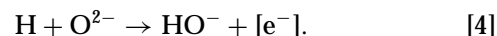
### 3.4. EPR and XPS

The EPR spectrum of a fresh  $YBa_2Cu_3O_7$  sample depicted in Fig. 2a exhibits a strong anisotropic signal with extremes at  $g_1 = 2.231$ ,  $g_2 = 2.130$ , and  $g_3 = 2.053$ , which are typical features of  $Cu^{2+}$  (46, 47). The broad line and the unresolved hyperfine structure are due to interaction among the  $Cu^{2+}$  species: the signal is broadened by magnetic dipolar interactions (and possibly, some spin exchange) between neighbouring paramagnetic ions. When  $YBa_2Cu_3O_7$  was heated at  $800^\circ C$  in He, a signal centered at  $g = 2.005$  (Fig. 2b) appeared, which could be attributed to  $e^-$  formed at the sites of surface oxygen vacancies in  $YBa_2Cu_3O_7$  according to the mechanism

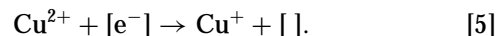


in which  $[ ]$  represents oxygen vacancies.

Figure 2c shows the EPR spectrum of  $YBa_2Cu_3O_7$  after the sample was reduced in  $H_2$  at  $250^\circ C$ . One can observe that the intensity of the  $Cu^{2+}$  signal decreased dramatically after reduction, indicating the partial reduction of  $Cu^{2+}$  to  $Cu^+$ . The  $e^-$  signal at ca.  $g = 2.005$  was generated due to the reactions



The electrons,  $e^-$ , were located at the oxygen vacancies and can reduce  $Cu^{2+}$  to  $Cu^+$ :



The EPR features of  $Cu^{2+}$  were almost unchanged when  $CO_2$  was adsorbed on a nonreduced  $YBa_2Cu_3O_7$  sample

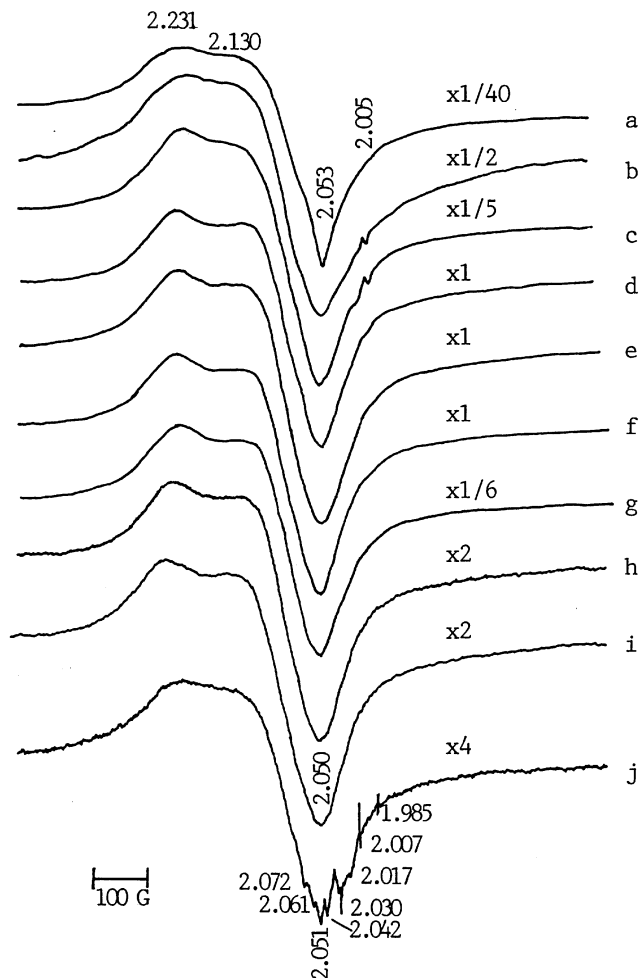
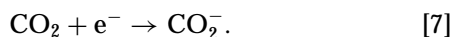
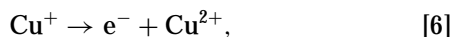


FIG. 2. EPR spectra of (a) fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, (b) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> heated at 800°C in He, (c) reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample exposed to (d) CO<sub>2</sub> at 250°C, (e) CO<sub>2</sub> at 300°C, (f) CO<sub>2</sub>/H<sub>2</sub> (3/1) at 250°C, (g) CO<sub>2</sub>/H<sub>2</sub> (1/1) at 250°C, (h) CO<sub>2</sub>/H<sub>2</sub> (1/3) at 250°C, CO<sub>2</sub>/H<sub>2</sub> (1/4) at 250°C, and (j) NO at 250°C.

at various temperatures. The Cu<sup>2+</sup> signal did not change in intensity either. However, CO<sub>2</sub> adsorption at 250 and 300°C on a reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample would cause the e<sup>-</sup> signal at ca. 2.005 to diminish (Figs. 2d and 2e), resulting in the oxidation of Cu<sup>+</sup> and formation of CO<sub>2</sub><sup>-</sup>, i.e.,



Mill *et al.* (48) and Solymosi *et al.* (49) reported that the adsorption of CO<sub>2</sub> on a cesium/silica surface and a K-modified Rh/SiO<sub>2</sub> surface would result in the formation of CO<sub>2</sub><sup>-</sup>.

Figures 2f–2i illustrated the EPR spectra after the reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample was exposed to a mixture of CO<sub>2</sub>/H<sub>2</sub> with molar ratios of 3/1, 1/1, 1/3, or 1/4, respectively. The e<sup>-</sup> signal disappeared in all the four spectra, implying that under a CO<sub>2</sub>- or H<sub>2</sub>-rich circumstance, the

trapped electrons can be consumed and redox reactions such as reactions [5] and [6] could have taken place in a CO<sub>2</sub>/H<sub>2</sub> atmosphere.

As we did not observe any 2100-G isotropic hyperfine splitting of Cu<sup>0</sup> atoms, we can be sure that there was no metallic copper in the sample (50). The adsorption of NO on a reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample would result in a EPR spectrum in which one can observe Cu<sup>+</sup>-NO species (Fig. 2j). This proves that Cu<sup>+</sup> existed (51, 52). Arakawa and Adachi suggested that the Cu<sup>2+</sup> and Cu<sup>+</sup> ions adjacent to the oxygen vacancies in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7- $\delta$</sub>  functioned as the active centers for the activation of NO (53). Comparison of the EPR spectrum of reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> to the EPR spectrum of a reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample exposed to N<sub>2</sub>O at 90°C showed no feature modification; this demonstrates that there were no Cu<sup>0</sup> atoms in the reduced sample and reaction [1] did not happen.

The XPS lines of the Cu(2p<sub>3/2</sub>) level of a YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample after various treatments are shown in Fig. 3. The fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample shows one peak with B.E. = 933.9 eV

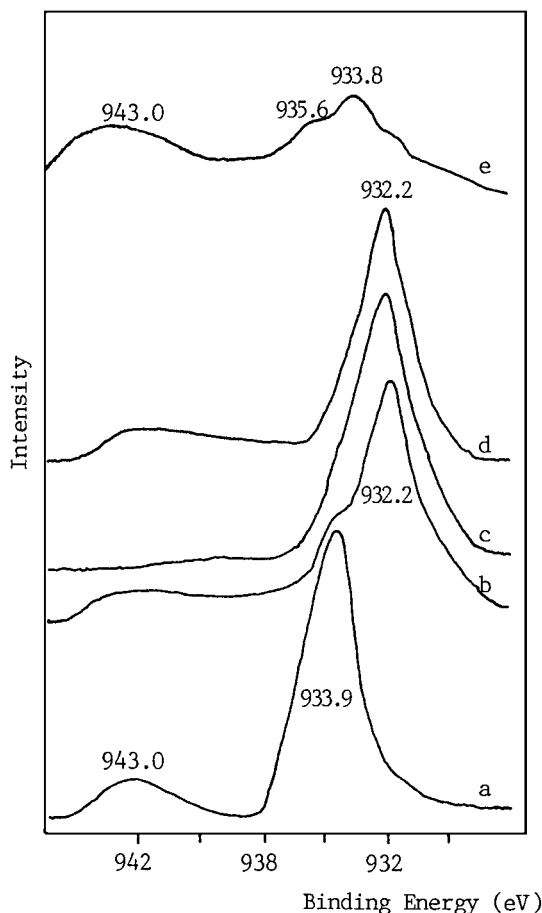


FIG. 3. Cu(2p<sub>3/2</sub>) XPS spectra of (a) fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, (b) reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, (c) reduced (H<sub>2</sub>, 400°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, (d) reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> exposed to CO<sub>2</sub>/H<sub>2</sub> (1/3) at 250°C, and (e) reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> after CO<sub>2</sub> TPD.

(Fig. 3a), which corresponds to  $\text{Cu}^{2+}$ . A satellite peak at 943.0 eV, which is a characteristic feature of  $\text{Cu}^{2+}$ , was also observed. After reduction at 250°C, the  $\text{Cu}(2p_{3/2})$  XPS spectrum shows a weak shoulder at B.E. = 933.9 eV and a strong peak at 932.2 eV which could be assigned to  $\text{Cu}^+$  or  $\text{Cu}^0$  (Fig. 3b). Together with the 933.9-eV peak, the satellite peak corresponding to  $\text{Cu}^{2+}$  reduced in intensity. After further reduction at 400°C, only the peak at 932.2 eV remained (Fig. 3c). Exposure of a sample reduced at 250°C to a reaction mixture of  $\text{CO}_2$  and  $\text{H}_2$  at 250°C could also result in a peak at 932.2 eV (Fig. 3d). After the adsorption and desorption of  $\text{CO}_2$  in a  $\text{CO}_2$ -TPD study, a profile with three components at ca. 935.6, 933.8, and 932.2 eV, and a satellite peak at 943.0 eV was observed. The highest peak intensity was at ca. 933.8 eV (Fig. 3e), indicating that  $\text{CO}_2$  can oxidize  $\text{Cu}^+$  to  $\text{Cu}^{2+}$ . Usually, the signal at B.E. = 935.6 eV is assigned to tetrahedrally coordinated  $\text{Cu}^{2+}$  sites while that at about 933.8 eV is assigned to octahedrally coordinated  $\text{Cu}^{2+}$  sites (54, 55). The distinction between the  $\text{Cu}^+$  and  $\text{Cu}^0$  cannot be confirmed solely on the basis of the B.E. of the  $\text{Cu}(2p_{3/2})$  level (56). We had turned to the X-ray-induced Cu LMM Auger line for final confirmation. After reduction, the Auger profile of a fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample changed from a broad peak centered at 918.0 eV (K.E.) to a strong peak centered at 917.2 eV (K.E.) with two shoulders at 918.1 eV (K.E.) and 918.6 eV (K.E.). According to the approach of Okamoto *et al.* (56), we concluded that it was  $\text{Cu}^+$  rather than  $\text{Cu}^0$  that existed on the surface of  $\text{YBa}_2\text{Cu}_3\text{O}_7$  after  $\text{H}_2$  reduction at 250°C.

### 3.5. $\text{O}_2$ TPD

Figure 4 shows the  $\text{O}_2$ -TPD profiles of fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  and reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$ . For a fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample, there was large  $\text{O}_2$  desorption starting at ca. 600°C (Fig. 4a). Somorjai (57) reported that some oxides could be reduced slightly due to  $\text{O}_2$  desorption at high temperatures in vacuum. No apparent  $\text{O}_2$  desorption was observed over a reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample (Fig. 4b), but  $\text{H}_2\text{O}$  ( $m/z = 18$ ) intensity increased with temperature rise (Fig. 4c). These indicate that, after reduction, there were H atoms left in the catalyst, which reacted with oxygen to give water.

### 3.6. $\text{CO}_2$ TPD

The  $\text{CO}_2$ -TPD profiles of a fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample exposed to  $\text{CO}_2$  at 200, 250, or 350°C are shown in Fig. 5A. According to the profile of desorption for  $\text{CO}_2$  adsorption at 200°C (Fig. 5A(a)), there could be three types of basic sites on the  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample:  $\text{CO}_2$  desorptions at the ranges of (i) <300°C, (ii) 300–500°C, and (iii) >600°C. The desorption of  $\text{CO}_2$  above 600°C is attributed to carbonates decomposition. The  $\text{CO}_2$ -TPD profiles of a reduced ( $\text{H}_2$ , 250°C)  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample exposed to  $\text{CO}_2$  at 200, 250, 300, or 400°C (Fig. 5B) exhibited very different features relative

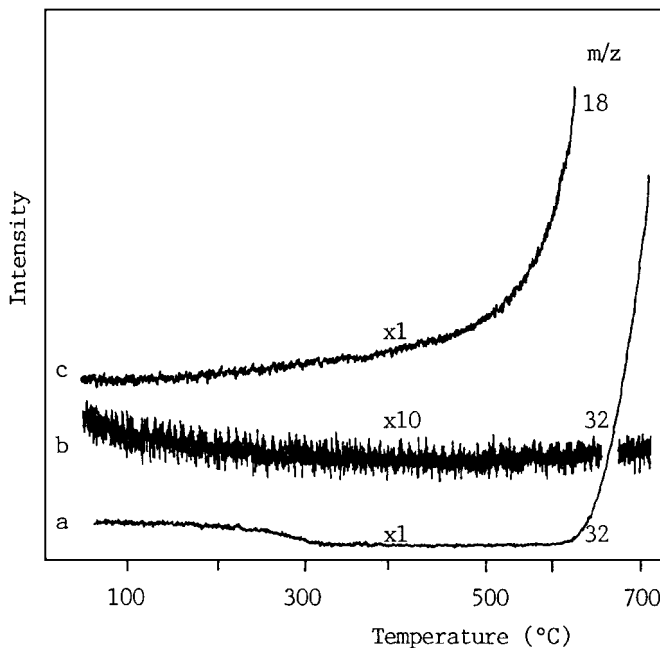


FIG. 4.  $\text{O}_2$  ( $m/z = 32$ ) desorption over (a) fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  and (b) reduced ( $\text{H}_2$ , 250°C)  $\text{YBa}_2\text{Cu}_3\text{O}_7$ ; (c)  $\text{H}_2\text{O}$  ( $m/z = 18$ ) desorption on reduced ( $\text{H}_2$ , 250°C)  $\text{YBa}_2\text{Cu}_3\text{O}_7$  during  $\text{O}_2$ -TPD performance.

to those of a fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample. There was only one  $\text{CO}_2$  desorption peak, implying that there was only one kind of basic site on the reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample. The desorption temperatures were 227, 280, 340, and 420°C (peak area was in turn increased) for  $\text{CO}_2$  adsorptions at 200, 250, 300, and 400°C, respectively. Comparing to the  $\text{CO}_2$ -TPD profile of a nonreduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample, the obvious difference is that there was no  $\text{CO}_2$  desorption at temperatures above 600°C, indicating that there was no carbonate formation when  $\text{CO}_2$  adsorbed on a reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample.

### 3.7. $\text{CO}_2$ TPSR

The  $\text{CO}_2$ -TPSR experiment was performed with a sample exposed (at 250°C) to  $\text{CO}_2$  being heated in a flow of  $\text{H}_2$ . The spectra are shown in Fig. 6. There were  $\text{CO}_2$  desorptions at ca. 80, 150, 200, 330, and above 620°C. Comparing to the results in Fig. 5B, we found that the intensity of  $\text{CO}_2$  desorption at around 320°C was very low and there was still a little  $\text{CO}_2$  desorption above 600°C, indicating that there was carbonate or bicarbonate formation when  $\text{H}_2$  reacted with the adsorbed  $\text{CO}_2$ . We observed that there were  $\text{CO}$  and  $\text{H}_2\text{O}$  desorptions above ca. 600°C, an indication of the occurrence of the RWGS reaction. In the  $\text{CD}_3\text{I}$  trapping experiments,  $\text{CD}_3\text{COOH}$  ( $m/z = 63$ ) and  $\text{CD}_3\text{OCH}_3$  ( $m/z = 49$ ) were detected from 80 to 360°C, whereas  $\text{CD}_3\text{CHO}$  ( $m/z = 47$ ) was detected only above 260°C during TPSR experiments. These imply

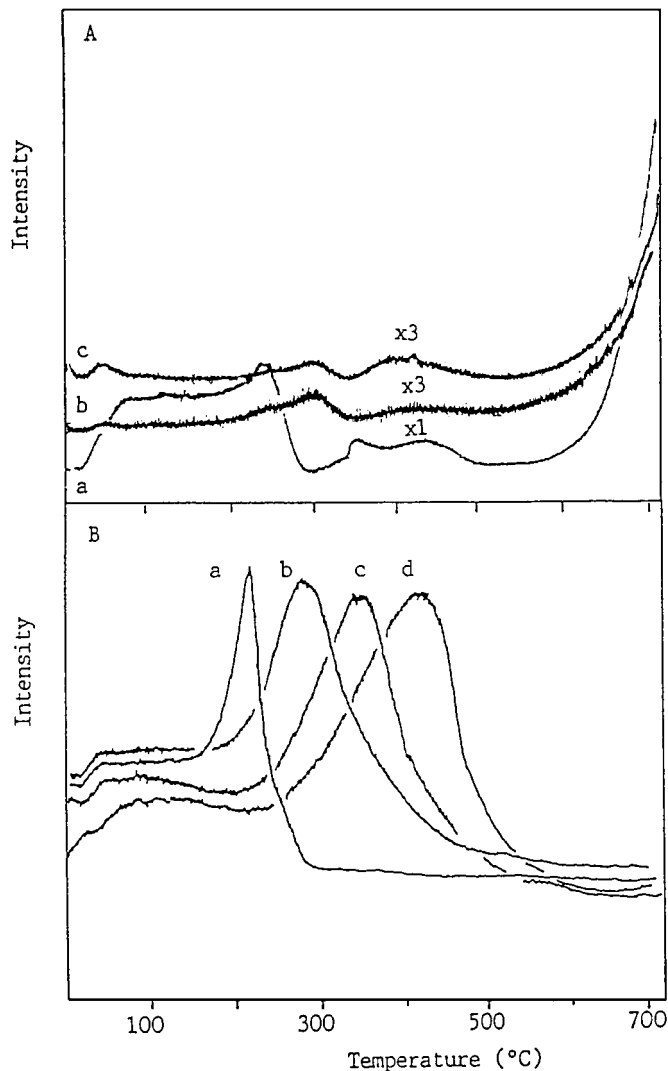


FIG. 5. (A) CO<sub>2</sub>-TPD profiles over fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> with CO<sub>2</sub> adsorbed at (a) 200°C, (b) 250°C, and (c) 350°C. (B) CO<sub>2</sub>-TPD profiles over reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> with CO<sub>2</sub> adsorbed at (a) 200°C, (b) 250°C, (c) 300°C, and (d) 400°C.

that formyl, formate, and methoxy were generated in CO<sub>2</sub> hydrogenation and formate generation was more feasible than formyl production.

### 3.8. Pulse Studies

MS spectra of CO<sub>2</sub> pulse studies at 250°C over the reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample with H<sub>2</sub> as the carrier gas are shown in Fig. 7. There was almost no CO<sub>2</sub> detection for the first three CO<sub>2</sub> pulses, indicating that most of the CO<sub>2</sub> molecules were adsorbed on the catalyst and were difficult to desorb. At the 11th pulse, the peak area of CO<sub>2</sub> reached the highest value. When CD<sub>3</sub>I was injected during CO<sub>2</sub> pulsing in H<sub>2</sub>, we detected CD<sub>3</sub>OCH<sub>3</sub> and CD<sub>3</sub>COOH. The result indicates that formate and methoxide were generated during CO<sub>2</sub> hydrogenation.

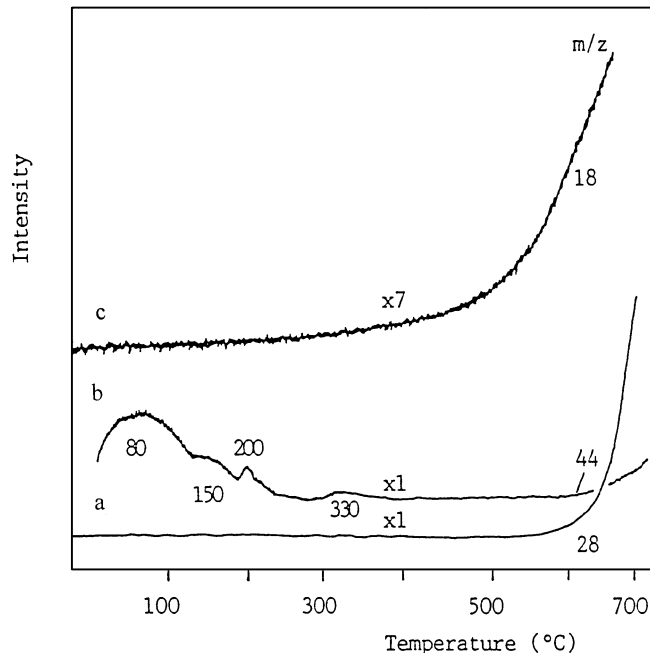


FIG. 6. Desorption of species with  $m/z =$  (a) 28 (CO), (b) 44 (CO<sub>2</sub>), and (c) 18 (H<sub>2</sub>O) during TPSR (CO<sub>2</sub>, H<sub>2</sub>) performed on reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>.

### 3.9. In Situ FTIR

**3.9.1. Fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> and reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>.** Figure 8 shows the *in situ*-FTIR spectra of the fresh and reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> samples. After reduction, the OH<sup>-</sup> band at ca. 3500 cm<sup>-1</sup> increased in intensity (Fig. 8b). The absorption bands at 677, 556, and 430 cm<sup>-1</sup> are due to in-plane oxygen motion, out-of-plane Cu motion, and out-of-plane oxygen motion, respectively (58a). One should take into consideration that the stretching of Cu-O-Cu in a tetragonal phase is somewhat different from that in an orthorhombic phase. Both YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> and La<sub>2</sub>CuO<sub>4</sub> have perovskite-related structures. In La<sub>2</sub>CuO<sub>4</sub>, if metallic copper existed, the in-plane mode response at 677 cm<sup>-1</sup> would be completely shielded (58a). In Figs. 8a and 8b, the

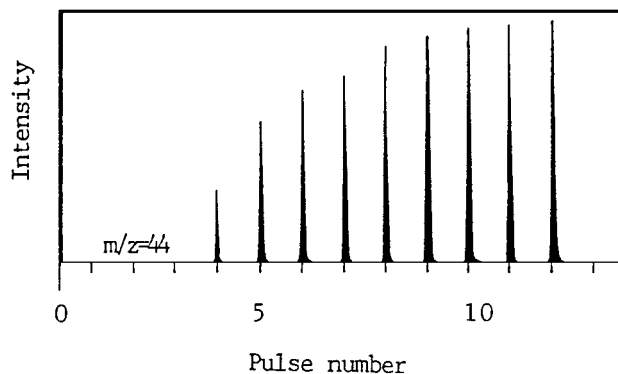


FIG. 7. Transient response of species with  $m/z = 44$  (CO<sub>2</sub>) during CO<sub>2</sub> pulsing on reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> with H<sub>2</sub> being the carrier gas.

bands at  $677\text{ cm}^{-1}$  are not shielded; we suggest that there was no metallic copper atom in both the fresh and reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  samples.

**3.9.2.  $\text{CO}_2$  and  $\text{H}_2$  adsorptions on fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$ .** Based on the interpretations in Refs. 33, 48, 49, and 58b–66, IR bands are assigned to various species as indicated in Table 4. The FTIR spectrum for  $\text{H}_2/\text{CO}_2$  (3:1, 3.0 MPa) adsorbed on a fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample at  $250^\circ\text{C}$  was recorded as shown in Fig. 9a. The bands attributable to ionic ( $1450\text{ cm}^{-1}$ ), bidentate carbonates ( $1563\text{ cm}^{-1}$ ), and bidentate bicarbonates ( $1610\text{ cm}^{-1}$ ) species were detected.

**3.9.3.  $\text{CO}_2$  and  $\text{H}_2$  adsorptions on reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$ .** Figure 9b shows the FTIR spectrum obtained by flowing  $\text{CO}_2$  over a reduced ( $\text{H}_2$ ,  $250^\circ\text{C}$ )  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample at  $250^\circ\text{C}$  and at 3.0 MPa for 0.5 h. The bands attributable to ionic, bidentate carbonates, monodentate ( $1360\text{ cm}^{-1}$ ) and bidentate ( $1535, 2849, 2922\text{ cm}^{-1}$ ) formates, hydroxide ( $3361\text{ cm}^{-1}$ ), bidentate methylenebisoxo ( $2970, 2868\text{ cm}^{-1}$ ),  $\text{CO}_2^-$  anion species ( $1325, 1695\text{ cm}^{-1}$ ), and C–O–C stretching ( $915, 1060\text{ cm}^{-1}$ ) were observed. With the rise in  $\text{CO}_2$  adsorption temperature to  $350^\circ\text{C}$ , bands attributable to methyl formate ( $1658, 1731\text{ cm}^{-1}$ ), ionic carbonate,  $\text{CO}_2^-$ , and hydroxide were observed; the bands due to bidentate formate and bidentate methylenebisoxo were dramatically weakened. Nevertheless, a broad band with weak intensity attributable to  $\text{CO}-\text{Cu}^+$  ( $2130\text{ cm}^{-1}$ ) was detected (Fig. 9c). The FTIR spectrum presented in Fig. 9d shows that after  $\text{H}_2/\text{CO}_2$  (3:1, 3.0 MPa) adsorption at  $250^\circ\text{C}$ , the bands

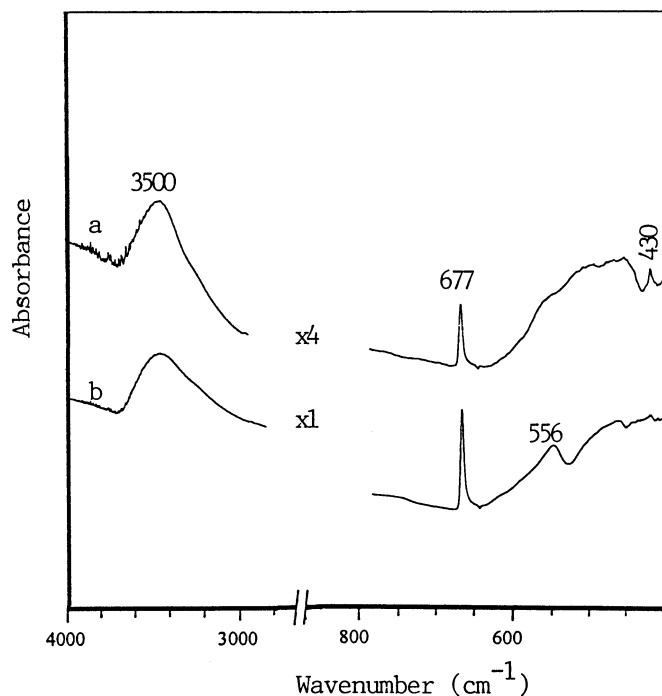


FIG. 8. Infrared spectra of (a) fresh  $\text{YBa}_2\text{Cu}_3\text{O}_7$  and (b) reduced ( $\text{H}_2$ ,  $250^\circ\text{C}$ )  $\text{YBa}_2\text{Cu}_3\text{O}_7$ .

TABLE 4  
Assignments of FTIR Absorbance Bands

Wavenumber ( $\text{cm}^{-1}$ )	Assignment	References
1605	$\text{H}_2\text{O}_{(a)}$	33
1450	$i\text{-CO}_{3(a)}$ (ionic carbonate)	59
1371, 1461	$m\text{-CO}_{3(a)}$ (monodentate carbonate)	59
1405	$p\text{-CO}_{3(a)}$ (polydentate carbonate)	59, 60
1563	$b\text{-CO}_{3(a)}$ (bidentate carbonate)	60
1610	$b\text{-HCO}_{3(a)}$ (bidentate bicarbonate)	60
1535, 2849, 2922	$b\text{-HCOO}_{(a)}$ (bidentate formate)	61, 60
1360	$m\text{-HCOO}_{(a)}$ (monodentate formate)	61, 60
2957	$\text{CH}_3\text{O}_{(a)}$ (methoxide)	64, 33
2970, 2868	$b\text{-CH}_2\text{OO}_{(a)}$ (bidentate methylenebisoxo)	62
3361	$\text{OH}_{(a)}$ (hydroxide)	33
1730, 2707, 2880	$\text{CH}_2\text{O}_{(a)}$ (formaldehyde), $\text{HCO}_{(a)}$ (formyl)	33, 66
1658, 1731	$\text{CH}_3\text{OCHO}_{(a)}$ (methyl formate)	64, 65
1695	$\text{CO}_2^-$ (antisymmetric stretch)	48, 49
1325	$\text{CO}_2^-$ (symmetric stretch)	48, 49
2130	$\text{CO}_{(a)}-\text{Cu}^+$ (linear adsorbed CO on $\text{Cu}^+$ )	63
2077	$\text{CO}_{(a)}-\text{Cu}$ (linear adsorbed CO on $\text{Cu}^0$ )	63
915, 1060	C–O–C (stretch)	58(b), 66

Note. (a) means adsorbed.

ascribed to bidentate formate, methoxide ( $2957\text{ cm}^{-1}$ ), methylenebisoxo, formyl and formaldehyde ( $1763, 2707, 2880\text{ cm}^{-1}$ ),  $\text{CO}_2^-$ , and C–O–C stretching were clearly observed.

### 3.10. FT-Raman

Figure 10 shows the laser FT-Raman spectra of a reduced ( $\text{H}_2$ ,  $250^\circ\text{C}$ )  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample exposed to a mixture of  $\text{CO}_2$  and  $\text{H}_2$  at various temperatures. At  $200$  and  $250^\circ\text{C}$ , the vibration bands at  $2870, 2940,$  and  $2970\text{ cm}^{-1}$  attributable to  $\text{CH}_x$ , at  $2574\text{ cm}^{-1}$  ascribed to formate and at  $1900\text{ cm}^{-1}$  ascribed to  $\text{C}=\text{O}$  (58b, 66) were obviously detected. With the increase of adsorption temperature, these bands decreased in intensity and almost disappeared at  $500^\circ\text{C}$ . The  $\text{CH}_x$  bands were hard to be detected above  $300^\circ\text{C}$ . Bands at ca.  $2300\text{ cm}^{-1}$  attributable to adsorbed  $\text{CO}_2$  and weak bands at ca.  $2100\text{ cm}^{-1}$  attributable to linear adsorbed CO were detected and their intensities decreased with temperature rise. These indicate that the hydrogenation of adsorbed  $\text{CO}_2$  to produce species containing C, H, and O atoms is unlikely to occur at high temperatures.

## 4. DISCUSSION

### 4.1. Composition and Active Phase of Catalyst

The orthorhombic  $\text{YBa}_2\text{Cu}_3\text{O}_7$  and tetragonal  $\text{YBa}_2\text{Cu}_3\text{O}_6$  structures are shown in Fig. 11. They consist of an



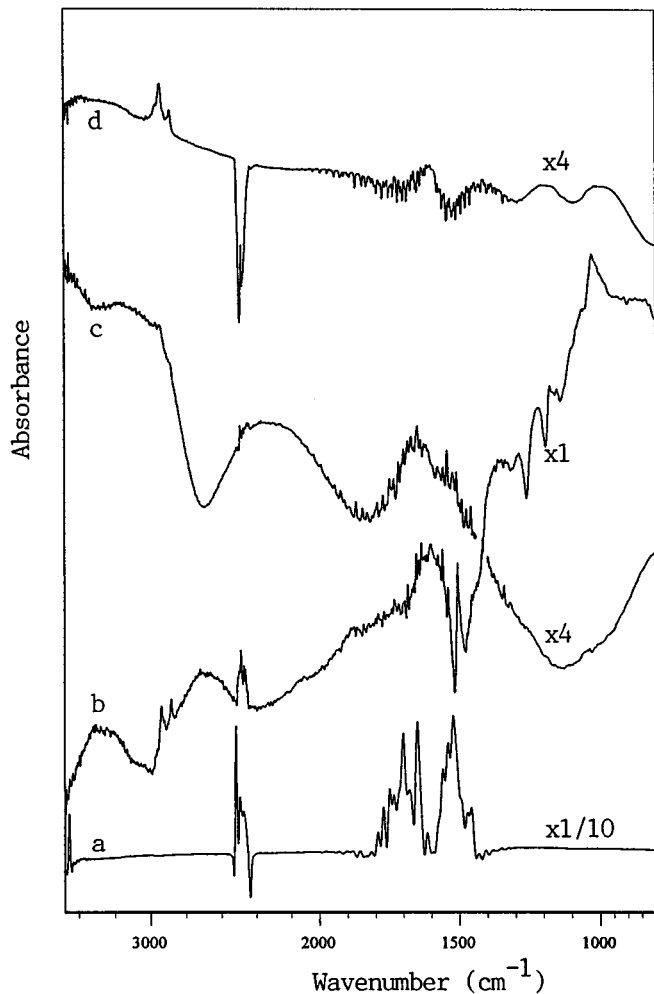


FIG. 9. Infrared spectra of (a) fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> exposed to H<sub>2</sub>/CO<sub>2</sub> (3:1, 3.0 MPa) at 250°C (spectrum was referenced to that of fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>); reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> exposed to (b) CO<sub>2</sub> (3.0 MPa) at 250°C, (c) CO<sub>2</sub> (3.0 MPa) at 300°C, and (d) H<sub>2</sub>/CO<sub>2</sub> (3:1, 3.0 MPa) at 250°C (spectra were referenced to that of reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>).

intergrowth sequence along the *c* axis:



In the layers of  $|\text{Cu}(2)\text{O}_2\text{-Y-Cu}(2)\text{O}_2|$ , there are two CuO<sub>2</sub> sheets. In the layers of  $|\text{BaO-Cu}(1)\text{O}_x\text{-BaO}|$ , there is a variable oxygen content in CuO<sub>*x*</sub>. The O<sub>*x*</sub> is rather sensitive to the structures and physical properties of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>. When *x* is close to 1, it is a superconductor with orthorhombic structure; when *x* is smaller than 0.5, it is an insulator with tetragonal structure. Under 1 atm of O<sub>2</sub>, the upper limit of *x* in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6+*x*</sub> is about 0.96 (43). The Cu(2) in the CuO<sub>2</sub> sheets are five-fold coordinated in both the orthorhombic and the tetragonal structures. The Cu(1) in the CuO<sub>*x*</sub> plane is four-fold coordinated in the orthorhombic structure and two-fold coordinated in the tetragonal structure. In tetragonal YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub>, the *c* axis oxygen

atoms are closer to the Cu(1) atoms in the CuO<sub>*x*</sub> plane than to the Cu(2) atoms of a CuO<sub>2</sub> sheet. As *x* increases, the *c* axis oxygen moves away from the Cu(1) toward the Cu(2) atoms. In YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6+*x*</sub>, the content of oxygen (*x*) varies and the distribution of the formal oxidation states of copper atoms is controlled by the oxygen coordination at the Cu atoms. When the Cu(1) atoms are linearly coordinated by two oxygen atoms, as in the Cu(1) planes of the YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub> with tetragonal structure, the copper atoms bear a formal valence Cu<sup>+</sup>. When the copper atoms are coordinated by five oxygen atoms, as in the Cu(2)O<sub>2</sub> sheets, the copper atoms may bear a formal valence Cu<sup>(2+*d*)</sup>, where *d* = 0 in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub> and *d* = 0.5 in ideal YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>. Baetzold observed the localized small polarons of Cu<sup>3+</sup> and O<sup>-</sup> when studying the electronic defects of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> (67). The Cu(1) atoms coordinated by four coplanar oxygen atoms in the orthorhombic structure are in the valence of +2; whereas the Cu(1) atoms coordinated by two-fold oxygen atoms in the tetragonal structure are in the valence of +1. The oxygen atoms of the Cu(1)O<sub>*x*</sub> planes become mobile above 300°C (68). It is therefore feasible to remove oxygen progressively in the temperature interval 300 < *T* ≤ 900°C (69). It is possible to vary *x* in the 0 ≤ *x* ≤ 0.96 range by changing the synthesis condition

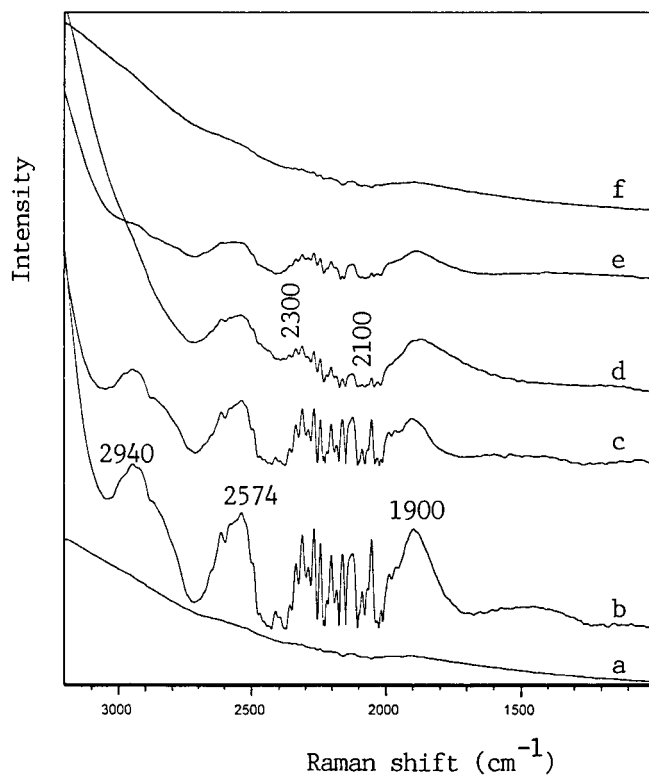


FIG. 10. FT-Raman spectra of reduced (H<sub>2</sub>, 250°C) YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> exposed to (a) N<sub>2</sub> at 250°C, (b) H<sub>2</sub>/CO<sub>2</sub> (3:1) at 200°C, (c) H<sub>2</sub>/CO<sub>2</sub> (3:1) at 300°C, (d) H<sub>2</sub>/CO<sub>2</sub> (3:1) at 400°C, (e) H<sub>2</sub>/CO<sub>2</sub> (3:1) at 400°C, and (f) H<sub>2</sub>/CO<sub>2</sub> (3:1) at 500°C.

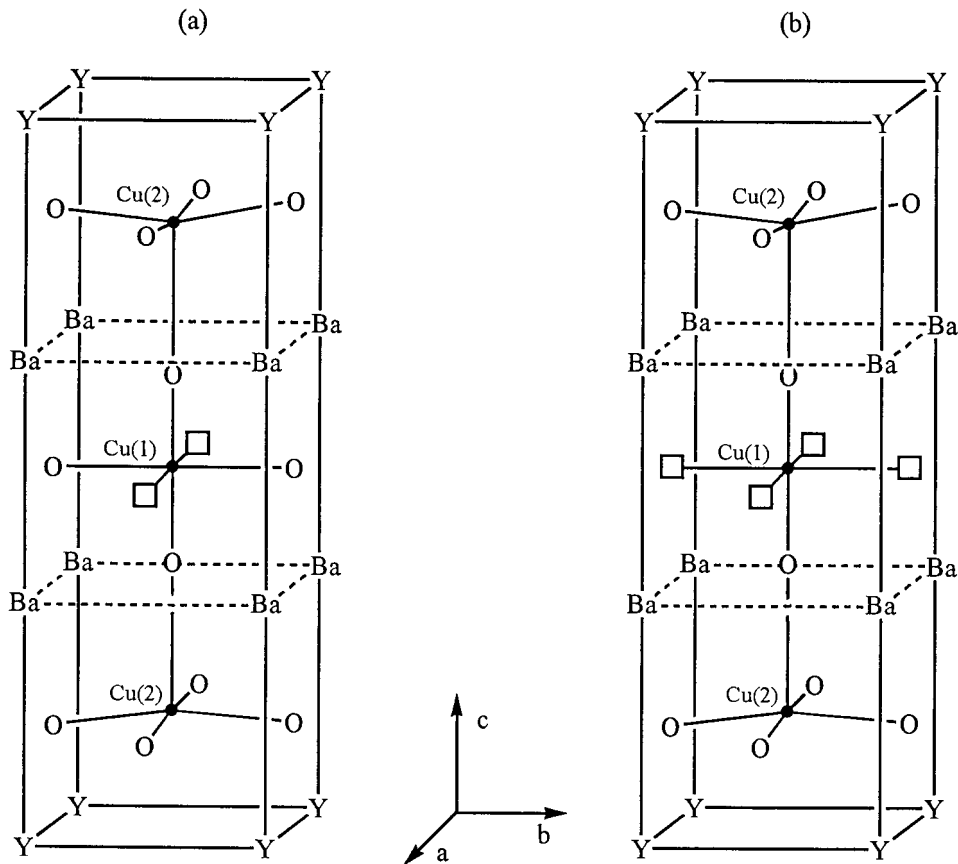


FIG. 11. Unit cell of (a) orthorhombic  $\text{YBa}_2\text{Cu}_3\text{O}_7$  and (b) tetragonal  $\text{YBa}_2\text{Cu}_3\text{O}_6$ . Note:  $\square$  denotes an oxygen vacancy with a trapped electron.

(70). Cava *et al.* (71) reported that there were  $\text{O}-\text{Cu}^+-\text{O}$  entities in  $\text{YCuO}_2$ .

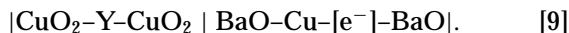
A reduced  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample with tetragonal phase showed activity in  $\text{CO}_2$  hydrogenation whereas a fresh one with orthorhombic phase did not. It indicated that the tetragonal phase is suitable for  $\text{CO}_2$  hydrogenation.  $\text{H}_2$ -TG/DTA results (Fig. 1A) illustrated that, after reduction at  $250^\circ\text{C}$ ,  $\text{YBa}_2\text{Cu}_3\text{O}_7$  has an average composition of  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ . The density of oxygen vacancies in the  $\text{CuO}_x$  plane of  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$  is less than that in a typical tetragonal structure of  $\text{YBa}_2\text{Cu}_3\text{O}_6$ . In other words, one can say that the number of coordinated oxygens is a little bit more than 2 in the  $\text{CuO}_x$  plane of  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ . In the orthorhombic structure of  $\text{YBa}_2\text{Cu}_3\text{O}_7$ ,  $\text{Cu}^{2+}$  and  $\text{Cu}^{3+}$  co-exist; part of the Cu in the  $\text{CuO}_x$  layer is five-fold coordinated. In the tetragonal structure of  $\text{YBa}_2\text{Cu}_3\text{O}_6$ ,  $\text{Cu}^+$  and  $\text{Cu}^{2+}$  co-exist; most of the Cu(1) in the  $\text{CuO}_x$  layer is two-fold coordinated. When  $\text{YBa}_2\text{Cu}_3\text{O}_7$  was reduced at  $250^\circ\text{C}$ , it changed to  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ , in which  $\text{Cu}^{2+}$  and  $\text{Cu}^+$  co-exist; the Cu(1) in the  $\text{CuO}_x$  layer is two- and/or three-fold coordinated. So far, there is no evidence to support that  $\text{Cu}^0$  can exist in a tetragonal structure of  $\text{YBa}_2\text{Cu}_3\text{O}_6$ .  $\text{N}_2\text{O}$  titration results suggested that there is no detectable metallic copper in tetragonal  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ . A  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$

sample exposed to  $\text{N}_2\text{O}$  at  $90^\circ\text{C}$  showed no change in EPR feature as compared to that of pure  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ . The XPS spectra (Fig. 3b) illustrated that after  $\text{H}_2$ -reduction at  $250^\circ\text{C}$ , the concentration of  $\text{Cu}^{2+}$  decreased. X-ray-induced Auger examination confirmed that  $\text{Cu}^+$ , rather than  $\text{Cu}^0$ , existed in the  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$  sample. When NO was adsorbed on  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ , there was a  $\text{NO}-\text{Cu}^+$  EPR signal (Fig. 2j). All these phenomena indicate that there were  $\text{Cu}^+$  ions but very little  $\text{Cu}^0$  in  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ . Rojas *et al.* (72, 73) demonstrated that the  $\text{Cu}^{2+}$  ions placed in a perovskite lattice come to be reduced at temperatures much higher than that in massive  $\text{CuO}$ . In other words, the extent of  $\text{Cu}^{2+}$  reduction in  $\text{YBa}_2\text{Cu}_3\text{O}_7$  is restricted. Brown-Bourzutschky *et al.* (74) reported that  $\text{Cu}^+$  in  $\text{LaM}_{1-x}\text{Cu}_x\text{O}_3$  ( $M = \text{Cu}, \text{Ti}$ ) should be responsible for methanol synthesis from CO hydrogenation. The FTIR results in Fig. 8 indicated that the  $\text{Cu}-\text{O}-\text{Cu}$  bond stretching vibration has been modified after the reduction of  $\text{YBa}_2\text{Cu}_3\text{O}_7$ . When  $\text{YBa}_2\text{Cu}_3\text{O}_7$  was reduced to  $\text{YBa}_2\text{Cu}_3\text{O}_{6.325}$ , the structure transformed from orthorhombic to tetragonal. In other words, the oxygen atoms in the  $c$  axis had moved away from Cu(2) and got closer to Cu(1), resulting in the small changes in FTIR (Fig. 8) features. The TPR profile (Fig. 1B(b)) showed that after  $\text{H}_2$ -reduction at  $250^\circ\text{C}$ , the  $\text{YBa}_2\text{Cu}_3\text{O}_7$  sample still exhibited

H<sub>2</sub> consumption at 190°C, suggesting that the oxygen atoms in the CuO<sub>x</sub> plane of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> were more mobile than those of the fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>.

#### 4.2. Trapped Electrons and Oxygen Vacancies in Reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

The EPR spectra in Figs. 2b and 2c show that by YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> being heated at 800°C in He or being reduced at 250°C in H<sub>2</sub>, trapped electrons were generated. As mentioned before, it is reported that the oxygen atoms in the CuO<sub>x</sub> plane are mobile at temperatures above 300°C. Our O<sub>2</sub>-TPD results (Fig. 4a) of fresh YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> showed that O<sub>2</sub> desorption started at 600°C. In a helium atmosphere, if the sample was heated below 800°C, no EPR signal of trapped electrons was detected, indicating that only above 800°C, the *b* axis oxygen in the CuO<sub>x</sub> plane could be removed significantly from the lattice. Thus, electron and oxygen vacancies would be generated along the *b* axis (see reaction [2] and Fig. 11). No significant oxygen desorption had been detected in the O<sub>2</sub>-TPD profile of reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> (Fig. 4b), indicating that the oxygen atoms in the CuO<sub>2</sub> sheet are more stable than those in the CuO<sub>x</sub> plane. Oxygen in the *b* axis can be removed in H<sub>2</sub>-reduction at lower temperatures, resulting in the generation of trapped electrons and oxygen vacancies according to reactions [3] and [4]. The electrons trapped at oxygen vacancies formed F centers. Thus, the sequence [8] in YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> can be written as



#### 4.3. Surface Redox Properties of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

The catalytic behaviours of perovskite-type oxides (ABO<sub>3</sub>) are closely related to the redox abilities of the *B* site ions. EPR results (Fig. 2c) demonstrated that the typical signal of Cu<sup>2+</sup> ions dramatically decreased in intensity and the e<sup>-</sup> signal was generated after H<sub>2</sub> reduction at 250°C. XPS studies (Fig. 3b) showed that, after reduction, there were large reductions in the intensities of the Cu<sup>2+</sup> peak at 933.9 eV and the corresponding satellite peak at 943.0 eV. The H<sub>2</sub>-TG/DTA measurements (Fig. 1A) showed that, after reduction, the composition of the catalyst should be YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub>. All these pieces of evidence support the theory that Cu<sup>2+</sup> ions in a YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample could be reduced to a certain extent. After adsorption of CO<sub>2</sub> on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> at 250°C, the XPS results (Fig. 3e) illustrate that Cu<sup>2+</sup> increased in concentration; the EPR results (Figs. 2d and 2e) show that the e<sup>-</sup> signal disappeared. The TPR profile of a YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample used in CO<sub>2</sub> hydrogenation (Fig. 1B(c)) shows a H<sub>2</sub> consumption peak at 280°C. These are clear pieces of evidence to suggest that CO<sub>2</sub> can oxidize the Cu<sup>+</sup> in the CuO<sub>x</sub> plane of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> to Cu<sup>2+</sup>. The results suggest that redox reactions such as reactions [5] and [6] had occurred. The EPR

studies of CO<sub>2</sub>/H<sub>2</sub> interaction with YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> (Figs. 2f–2i) denote that no matter in a H<sub>2</sub>-rich or CO<sub>2</sub>-rich environment, there was no signal of trapped electrons. It suggests that, under the CO<sub>2</sub> hydrogenation conditions, CO<sub>2</sub> can take up a trapped electron and oxidize Cu<sup>+</sup> to Cu<sup>2+</sup>.

#### 4.4. CO<sub>2</sub> Adsorption and Reaction with Reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

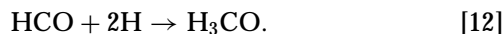
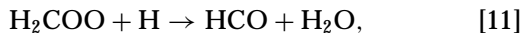
The CO<sub>2</sub>-TPD results shown in Fig. 5B indicate that there was one type of basic site on the surface of a reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> sample. We assume that the basic centers are the [e<sup>-</sup>] sites generated in H<sub>2</sub> reduction. The results in Figs. 5A and 5B and the FTIR spectra on CO<sub>2</sub> adsorption (Figs. 9a and 9b) also provide pieces of evidence that, after the reduction of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, the quantity of carbonates decreased, implying that the presence of trapped electrons and oxygen vacancies can hinder the formation of carbonates. FTIR (Fig. 9b) demonstrate that CO<sub>2</sub><sup>-</sup>, rather than CO, was formed during CO<sub>2</sub> adsorption on reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> at low temperature, indicating that CO<sub>2</sub> takes up a trapped electron and generates CO<sub>2</sub><sup>-</sup>. Considering the geometric and electronic effects, it is possible that CO<sub>2</sub> adsorption occurred on the oxygen vacancies in the CuO<sub>x</sub> plane of reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>. The oxygen atoms in CO<sub>2</sub> incorporated into the oxygen vacancies and took up a trapped electron, resulting in further oxidation of Cu<sup>+</sup> to Cu<sup>2+</sup> (see reactions [6] and [7]). In the FTIR spectrum of CO<sub>2</sub> adsorption on reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> (Fig. 9b), in addition to the CO<sub>2</sub><sup>-</sup>, CO<sub>3</sub>, and HCO<sub>3</sub> bands, there are bands corresponding to the HCOO and H<sub>2</sub>COO groups, indicating that formate and methylenebisoxo species were generated in the interaction of CO<sub>2</sub><sup>-</sup> with surface hydrogen.

#### 4.5. H<sub>2</sub> Reaction with CO<sub>2</sub> Adspecies on Reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

The TPSR results in Fig. 6 reveal that there were little CO<sub>2</sub> desorptions at 80, 150, 200, 330, and 650°C, indicating that the adsorbed CO<sub>2</sub> had been converted to carbonate or bicarbonate which decomposed to give CO<sub>2</sub> and H<sub>2</sub>O. FT-Raman spectra (Fig. 10) support the theory that the co-adsorption of CO<sub>2</sub> and H<sub>2</sub> would result in the generation of CH, CH<sub>2</sub>, and CH<sub>3</sub> groups. Above 600°C, CO desorption was observed, indicating that the RWGS reaction occurred at high temperatures. The *in situ*-FTIR spectrum (Fig. 9d) illustrates that, after the adsorptions of H<sub>2</sub> and CO<sub>2</sub>, the bands of OH, HCOO, H<sub>2</sub>COO, CH<sub>2</sub>O, HCO, CH<sub>3</sub>O, and CH<sub>3</sub>OCHO appeared, whereas compared to those of Fig. 9b, the intensities of the H<sub>2</sub>COO bands were weakened. The results indicate that the adsorbed hydrogen had reacted with H<sub>2</sub>COO; methanol and dimethyl ether were generated via the CH<sub>2</sub>O and HCO intermediates.

The results of pulsing CO<sub>2</sub> in a H<sub>2</sub> flow (Fig. 7) at 250°C show that there was one CO<sub>2</sub> response peak for each pulse.

In the initial CO<sub>2</sub> pulses, no peaks with  $m/z = 44$  were detected, implying that, in the presence of hydrogen, CO<sub>2</sub> adsorbed rather strongly on the catalyst. During CO<sub>2</sub> pulsing in H<sub>2</sub>, we trapped methoxy and formate. Both the FTIR and CD<sub>3</sub>I-trapping results imply that, in the presence of H<sub>2</sub>, (i) CO<sub>2</sub> adsorbs strongly on reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>; (ii) H<sub>2</sub>COO species can be transformed to other species; and (iii) HCOO is readily generated. The reaction between adsorbed hydrogen and CO<sub>2</sub> could be depicted as



The H<sub>2</sub>COO species is unstable and transformed easily to other intermediates such as formyl and methoxy in the presence of hydrogen. At higher temperatures, the formyl could be decomposed to CO. The fact that the absorbance band of methylenebisoxo was relatively weak in Fig. 9d supports the above speculation.

#### 4.6. Hydrogen Adsorption and Spillover on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

Previous work by Fujita *et al.* on a Cu/SiO<sub>2</sub> catalyst has shown that H<sub>2</sub> adsorbs dissociatively on copper with an adsorption heat of about 12 kcal mol<sup>-1</sup> and an activation barrier of about 10.5 kcal mol<sup>-1</sup> (75). Other studies on Cu/ZrO<sub>2</sub> catalysts suggest that Cu is more effective than ZrO<sub>2</sub> in dissociating H<sub>2</sub>, and Cu serves to adsorb H<sub>2</sub> dissociatively and to provide a source of atomic hydrogen (76–78). For YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, H<sub>2</sub> may adsorb preferably on the Cu<sup>+</sup> sites of CuO<sub>x</sub>, offering electrons to oxygen vacancies to form F centers, into which the oxygen atoms of CO<sub>2</sub> insert. The generation of HCOO, HCOOH, and H<sub>2</sub>COO is due to the interaction between the adsorbed H and adsorbed CO<sub>2</sub> by means of H spillover. Fisher *et al.* proposed a methanol synthesis mechanism of CO<sub>2</sub> hydrogenation on Cu/ZrO<sub>2</sub>/SiO<sub>2</sub>, in which Cu and Zr are envisioned to be in close proximity (33). The H adsorbed on Cu can spill over to the carbonate on Zr to form HCOO and H<sub>2</sub>COO intermediates, leading finally to the production of methanol. In the CuO<sub>x</sub> plane of reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, if H<sub>2</sub> adsorbed on the Cu site and CO<sub>2</sub> adsorbed on the oxygen vacancies, there would be no blockage between the two. So the spillover of H to CO<sub>2</sub> to generate COOH and COHOH intermediates could be feasible. The COOH and COHOH species could rearrange to relatively more stable species, such as HCOO (formate) and H<sub>2</sub>COO (methylenebisoxo). Due to H spillover from Cu<sup>+</sup>, HCOO and H<sub>2</sub>COO species could transform to HCOOH, HCOHOH, H<sub>2</sub>COOH, and H<sub>2</sub>COHOH. The HCOHOH and H<sub>2</sub>COHOH intermediates could dehydrate to produce HCO (formyl) and H<sub>2</sub>CO (formaldehyde), which could be hydrogenated to H<sub>3</sub>CO (methoxide). In addition, the FT-Raman spectra (Fig. 10) illustrate that CH<sub>x</sub>

( $x = 1, 2,$  and  $3$ ) species were generated at 200 and 250°C, implying that the spillover of hydrogen proceeds rather efficiently.

#### 4.7. Reaction Intermediates of CO<sub>2</sub> Hydrogenation on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

Over copper catalysts, CO hydrogenation to methanol is known to occur via a formyl (CHO) intermediate, whereas the CO<sub>2</sub> hydrogenation to methanol involves a formate (HCOO) intermediate (79, 80). Clarke *et al.* suggested that methanol is formed via the stepwise hydrogenation of HCOO–Cu to methylenebisoxo, and the methoxide species is the final precursor to methanol on a Cu/SiO<sub>2</sub> catalyst (81). With the adsorption of CO<sub>2</sub> on reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>, bands of formate and methylenebisoxo were observed at 250°C (Fig. 9b). At 350°C, the formate bands almost disappeared and that of methylenebisoxo vanished, whereas the CO band appeared (Fig. 9c). It means that the intermediates, especially methylenebisoxo, are unstable at high temperatures. In other words, high temperatures are suitable for CO formation. The FT-Raman spectra in Fig. 10 illustrate that high temperature is unfavourable to the C–H and C=O formation. After CO<sub>2</sub> and H<sub>2</sub> adsorptions at 250°C, the FTIR bands of formate, formyl, formaldehyde, methoxide, and C–O–C appeared, but the band of methylenebisoxo was observed in low intensity (Fig. 9d). It indicates that, with more hydrogen spilled over to methylenebisoxo, the intermediate rearranged and decomposed.

#### 4.8. Possible Reaction Mechanism for CO<sub>2</sub> Hydrogenation to Methanol on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>

Based on the preceding arguments, a possible mechanism for CO<sub>2</sub> hydrogenation to methanol on reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> is presented in Fig. 12. In this scheme, H<sub>2</sub> and CO<sub>2</sub> adsorbed on Cu<sup>+</sup> and oxygen vacancies (with trapped electrons), respectively. The spillover of H from Cu<sup>+</sup> to the adsorbed CO<sub>2</sub> would lead to the formation of HCOO, HCOHOH, H<sub>2</sub>COO, H<sub>2</sub>COOH, and H<sub>2</sub>COHOH. The dehydration of HCOHOH and H<sub>2</sub>COHOH would give HCO (formyl) and H<sub>2</sub>CO (formaldehyde), respectively, which reacts with H to produce methanol.

#### 4.9. Catalytic Performance Interpretation

Tables 1–3 indicate that high pressure, high space velocity, and low temperature are favourable to methanol synthesis. The by-products of methanol synthesis are CO and CH<sub>3</sub>OCH<sub>3</sub>. In the FTIR spectra of CO<sub>2</sub> adsorption at 250°C (Fig. 9b), one cannot observe any band due to adsorbed CO on Cu, indicating that the dissociation of CO<sub>2</sub> to CO and O on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> is difficult. The dehydrogenation of H<sub>2</sub>CO and HCO in the CO<sub>2</sub> hydrogenation scheme (Fig. 12) may be responsible for the formation of CO. High pressure, low temperature, and high space velocity probably can suppress

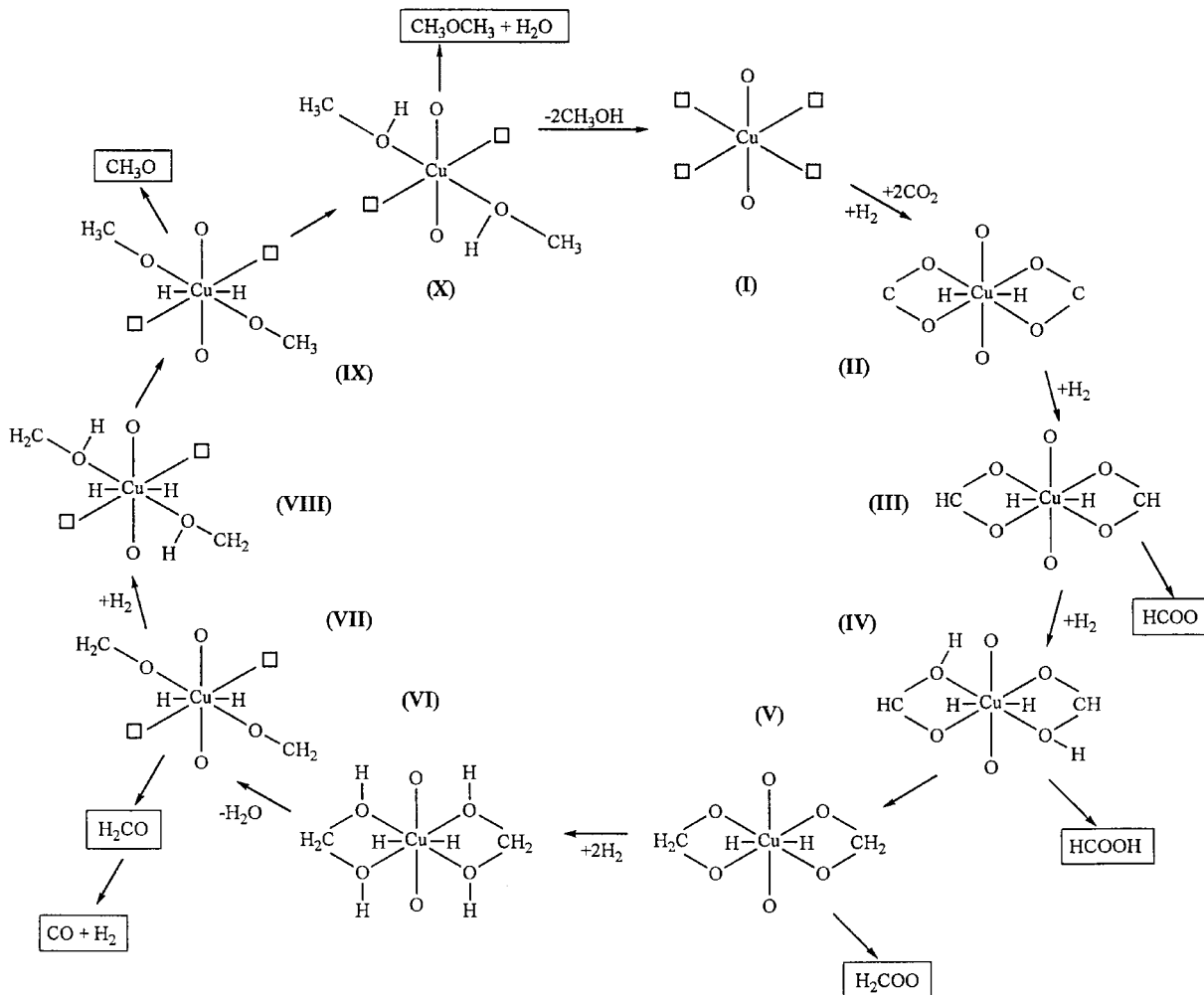


FIG. 12. Proposed mechanism for the synthesis of methanol from CO<sub>2</sub> and H<sub>2</sub> over tetragonal YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6</sub>.

the dehydrogenation of CH<sub>2</sub>O and HCO. Low temperature is suitable for hydrogen spillover to generate CH<sub>x</sub> ( $x=1, 2,$  and  $3$ ) functional groups for methanol production. The effect of reaction conditions on CH<sub>3</sub>OCH<sub>3</sub> production is similar to that on CH<sub>3</sub>OH, implying that both CH<sub>3</sub>OCH<sub>3</sub> and CH<sub>3</sub>OH are generated from the same intermediates. The CO<sub>2</sub>/H<sub>2</sub> adsorption FTIR spectrum (Fig. 9d) exhibits a band of C–O–C stretching. Hence, CH<sub>3</sub>OCH<sub>3</sub> may be formed from two CH<sub>3</sub>OH via a dehydration step on the surface of reduced YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub>.

## 5. CONCLUSIONS

YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> H<sub>2</sub>-reduced at 250 °C was active for methanol synthesis via CO<sub>2</sub> hydrogenation. After reduction, the structure of YBa<sub>2</sub>Cu<sub>3</sub>O<sub>7</sub> transformed from orthorhombic to tetragonal. The composition of the tetragonal structure is YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> in which Cu<sup>2+</sup> and Cu<sup>+</sup> co-exist with no metallic Cu<sup>0</sup>. In YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub>, there are trapped electrons

and oxygen vacancies. CO<sub>2</sub> adsorbed on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> could take up the trapped electrons, resulting in the oxidation of Cu<sup>+</sup> to Cu<sup>2+</sup>. Therefore, the redox between Cu<sup>+</sup> and Cu<sup>2+</sup> might play an important role in CO<sub>2</sub> hydrogenation. The intermediates of CO<sub>2</sub> hydrogenation were HCOO, H<sub>2</sub>COO, HCO, and H<sub>2</sub>CO species. We have proposed a mechanism for CO<sub>2</sub> hydrogenation on YBa<sub>2</sub>Cu<sub>3</sub>O<sub>6.325</sub> in which H<sub>2</sub> is dissociatively adsorbed on the Cu<sup>+</sup> site and CO<sub>2</sub> is adsorbed on the oxygen vacancies via its two oxygen atoms. The adsorbed CO<sub>2</sub> then undergoes stepwise hydrogenation to COOH, COHOH, HCOOH, HCOHOH, and H<sub>2</sub>COHOH with H being supplied by means of H spillover from Cu<sup>+</sup>. The intermediates COOH, COHOH, HCOHOH, and H<sub>2</sub>COHOH could transform to formate, methylenebisoxo, formyl, and formaldehyde groups, respectively. The final and crucial step in this sequence would be the hydrogenation of formyl and formaldehyde. The dehydrogenation of formyl and formaldehyde can produce CO, a major by-product in methanol synthesis.

## ACKNOWLEDGMENT

The work described above was fully supported by a grant from the Research Grants Council of the Hong Kong Special Administration Region, China (Project RGC/96-97/02).

## REFERENCES

- Kagan, Y. B., Liberov, L. G., Slivinskii, E. V., Loktev, S. M., Lin, G. T., Rozovskii, A. Y., and Bashkirov, A. N., *Dokl. Akad. Nauk. SSSR* **221**, 1093 (1975).
- Rozovskii, A. Y., Lin, G. T., Liberov, L. G., Slivinskii, E. V., Loktev, S. M., Kagan, Y. B., and Bashkirov, A. N., *Kinet. Katal.* **18**, 691 (1977).
- Rozovskii, A. Y., *Russ. Chem. Rev.* **58**, 41 (1987); *Kinet. Katal.* **21**, 97 (1980).
- Chinchen, G. C., Denny, P. J., Parker, D. J., Spenser, M. S., and Whan, D. A., *Appl. Catal.* **30**, 333 (1987).
- Chinchen, G. C., Mansfield, K., and Spenser, M. S., *CHEMTECH* **20**, 692 (1990).
- Chanchlani, K. G., Hudgins, P. R., and Silveston, P. L., *J. Catal.* **136**, 59 (1992).
- Sahibzada, M., Metcalfe, I. S., and Chadwick, D., *J. Catal.* **174**, 111 (1998).
- Liu, G., Willcox, D., Garland, M., and Kung, H. H., *J. Catal.* **90**, 139 (1984).
- Denise, B., Sneed, R. P. A., and Hamon, C., *J. Mol. Catal.* **17**, 339 (1982).
- Takegawa, M., and Ohsugi, M., *J. Catal.* **107**, 161 (1987).
- Lee, J. S., Lee, K. H., Lee, S. Y., and Kim, Y. G., *J. Catal.* **144**, 414 (1993).
- Klier, K., Chatikavanj, V., Herman, R. G., and Simmons, G. W., *J. Catal.* **74**, 343 (1982).
- Vedage, G. A., Pitchai, R., Herman, R. G., and Klier, K., "Proceedings, 8th International Congress on Catalysis, Berlin, 1984," Vol. II, p. 47. Dechema, Frankfurt-am-Main, 1984.
- Chinchen, G. C., Waugh, K. C., and Whan, D. A., *Appl. Catal.* **25**, 101 (1986).
- Robbins, J. L., Iglesia, E., Kelkar, C. P., and DeRites, B., *Catal. Lett.* **10**, 1 (1991).
- Klier, K., *Adv. Catal.* **31**, 243 (1982).
- Nonneman, L. E. Y., and Ponc, V., *Catal. Lett.* **7**, 213 (1990).
- Okamoto, Y., Fukino, K., Imanaka, T., and Eranishi, S., *J. Chem. Soc., Chem. Commun.* 1405 (1982); *J. Phys. Chem.* **87**, 3747 (1983).
- Frost, J. C., *Nature* **334**, 577 (1988).
- Rostrup-Nielsen, J. R., and Nielsen, H., "Deactivation and Poisoning of Catalysis" (J. Oudar and H. Wise, Eds.), p. 259. Dekker, New York, 1985.
- Clausen, B. S., Steffensen, G., Fabius, B., Villadsen, J., Feidenhans'l, R., and Topsøe, H., *J. Catal.* **132**, 524 (1991).
- Clausen, B. S., Schiøtz, J., Gråbæk, L., Ovesen, C. V., Jacobsen, K. W., Nøskov, J. K., and Topsøe, H., *Topics Catal.* **1**, 367 (1994).
- Clausen, B. S., Gråbæk, L., Steffensen, G., Hansen, P. L., and Topsøe, H., *Catal. Lett.* **20**, 23 (1993).
- Ovesen, C. V., Clausen, B. S., Schiøtz, J., Stoltze, P., Topsøe, H., and Nøskov, J. K., *J. Catal.* **168**, 133 (1997).
- Chinchen, G. C., Spenser, M. S., Waugh, K. C., and Whan, D. A., *J. Chem. Soc., Faraday Trans. 1* **83**, 2193 (1987).
- Chinchen, G. C., Waugh, K. C., and Whan, D. A., *Appl. Catal.* **25**, 101 (1986).
- Torras, J., Ricart, J. M., Illas, F., and Rubio, J., *Surf. Sci.* **297**, 57 (1993).
- Bagus, P. S., and Illas, F., *Phys. Rev. B* **42**, 10852 (1990).
- Muhler, M., Törnqvist, E., Nielsen, L. P., and Clausen, B. S., *Catal. Lett.* **25**, 1 (1994).
- Burch, R., Golunski, S. E., and Millar, G. J., *Catal. Lett.* **5**, 55 (1990).
- Bowker, M., Hadden, R. A., Houghton, H., Hyland, J. N., and Waugh, K. C., *J. Catal.* **109**, 263 (1988).
- Bowker, M., and Madix, R. J., *Surf. Sci.* **102**, 542 (1981).
- Fisher, I. A., and Bell, A. T., *J. Catal.* **172**, 222 (1997).
- Hayden, B. E., Prince, K., Woodruff, D. P., and Bradshaw, A. M., *Surf. Sci.* **133**, 589 (1983).
- Newsome, D. S., *Catal. Rev. Sci. Eng.* **21**, 275 (1980), and references therein.
- Waches, J. E., and Madix, R. J., *J. Catal.* **53**, 208 (1978).
- Gür, T. M., Wise, H., and Huggins, R. A., *Catal. Lett.* **23**, 387 (1994).
- Hansen, S., Otamiri, J., Bovin, J. O., and Andersen, A., *Nature* **334**, 143 (1988).
- Tabata, K., Fukui, H., Kohiki, S., Mizuno, N., and Misono, M., *Chem. Lett* **799** (1988).
- Mizuno, N., Yamato, M., and Misono, M., *J. Chem. Soc., Chem. Commun.* **887** (1988).
- Maeno, Y., Tomita, T., Kyogoku, M., Awaji, S., Aoki, Y., Hosino, K., and Fujita, T., *Nature* **328**, 512 (1987).
- Islam, M. S., and Baetzold, R. C., *Phys. Rev. B* **40**, 10926 (1989).
- Goodenough, J. B., and Manthiram, A., *J. Solid State Chem.* **88**, 115 (1990).
- Dandekar, A., and Vannice, M. A., *J. Catal.* **178**, 621 (1988).
- Schalten, J. J. F., and Konvalinka, J. A., *J. Chem. Soc., Faraday Trans.* **65**, 2465 (1969).
- Arias, A. M., Cataluña, R., Conesa, J. C., and Soria, J., *J. Phys. Chem. B* **102**, 809 (1998).
- Chao, C. C., and Lunsford, J. H., *J. Chem. Phys.* **57**, 2890 (1972).
- Millar, G. J., and Rochester, C. H., *Topics Catal.* **3**, 103 (1996).
- Solymosi, F., and Knözinger, H., *J. Catal.* **122**, 166 (1990).
- Kasai, P. H., and McLeod, D., *J. Chem. Phys.* **55**, 1566 (1971).
- Sojka, Z., Che, M., and Giamello, E., *J. Phys. Chem.* **97**, 305 (1997).
- Chao, C. C., and Lunsford, J. H., *J. Phys. Chem.* **76**, 1546 (1972).
- Arakawa, T., and Adachi, G., *Mater. Res. Bull.* **24**, 529 (1989).
- D'Huysser, A., Wrobel, G., and Bonnelle, J. P., *Nouv. J. Chim.* **6**, 437 (1982).
- D'Huysser, A., Le Calonnec, D., Lenglet, M., Bonnelle, J. P., and Jørgensen, C. K., *Mater. Res. Bull.* **19**, 1157 (1984).
- Okamoto, Y., Fukono, K., Imanaka, T., and Teranishi, S., *J. Phys. Chem. B* **87**, 3747 (1983).
- Somorjai, G. A., "Chemistry in Two Dimensions Surfaces." Cornell University Press, Ithaca, NY, 1981.
- Schrader, B., "Infrared and Raman Spectroscopy," (a) pp. 401-407, (b) pp. 190, 209, 212. VCH Verlagsgesellschaft mbH/VCH, Weinheim New York, 1995.
- Edwards, J. F., and Schrader, J. L., *J. Phys. Chem.* **88**, 5620 (1984).
- Hertl, W., *Langmuir* **5**, 96 (1989).
- Millar, G. J., Rochester, C. H., and Waugh, K. C., *J. Chem. Soc., Faraday Trans.* **87**, 1491 (1991).
- Stuve, E. M., Madix, R. J., and Sexton, B. A., *Surf. Sci.* **119**, 279 (1982).
- Clarke, D. B., Lee, D. K., Sandoval, M. J., and Bell, A. T., *J. Catal.* **142**, 27 (1993).
- Monti, D. M., Cant, N. W., Trimm, D. L., and Wainwright, M. S., *J. Catal.* **100**, 17 (1986).
- Millar, G. J., Rochester, C. H., and Waugh, K. C., *J. Chem. Soc., Faraday Trans.* **81**, 2785 (1991).
- Bellamy, L. J., "The Infrared Spectra of Complex Molecules," 3rd ed., Vol. 1, pp. 5-9, Chapman and Hall, London, 1986.
- Baetzold, R. C., *Phys. Rev. B* **38**, 11304 (1988).
- Manthiram, A., Swinnea, J. S., Sui, Z. T., Steinfink, H., and Goodenough, J. B., *J. Am. Chem. Soc.* **109**, 6667 (1987).
- Manthiram, A., and Goodenough, J. B., *Nature* **329**, 701 (1987).
- More, C., and Duran, P., "Properties and Applications of Perovskite-type Oxides" (L. G. Tejuca and J. L. G. Fierro, Eds.), p. 33. Marcel Dekker, Inc., New York, 1992.

71. Cava, R. J., Zandbergen, H. W., Ramirez, A. P., Takagi, H., Chen, C. T., Krajewski, J. J., Peck, W. F., Jr., Waszczak, J. V., Meigs, G., Roth, R. S., and Schneemeyer, L. F., *J. Solid State Chem.* **104**, 437 (1993).
72. Rojas, M. L., Fierro, J. L. G., Tejuca, L. G., and Bell, A. T., *J. Catal.* **124**, 41 (1990).
73. Rojas, M. L., Fierro, J. L. G., and Tejuca, L. G., *J. Solid State Chem.* **89**, 299 (1990).
74. Brown-Bourzutschky, J. A., Homs, N., and Bell, A. T., *J. Catal.* **124**, 52 (1990).
75. Fujita, S., Usui, M., Ito, H., and Takezawa, N., *J. Catal.* **157**, 403 (1995).
76. Fisher, I. A., Woo, H. C., and Bell, A. T., *Catal. Lett.* **44**, 11 (1997).
77. Burch, R., Golunski, S. E., and Spencer, M. S., *J. Chem. Soc., Faraday Trans.* **86**, 2683 (1990).
78. He, M. Y., and Ekerdt, J. G., *J. Catal.* **90**, 17 (1984).
79. Bart, J. C. J., and Sneed, R. P. A., *Catal. Today* **2**, 1 (1987).
80. Tagawa, T., Pleizier, G., and Amenomiya, Y., *Appl. Catal.* **18**, 285 (1985).
81. Clarke, D. B., and Bell, A. T., *J. Catal.* **154**, 314 (1995).